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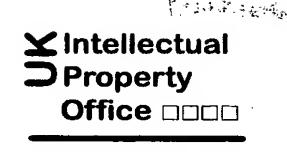
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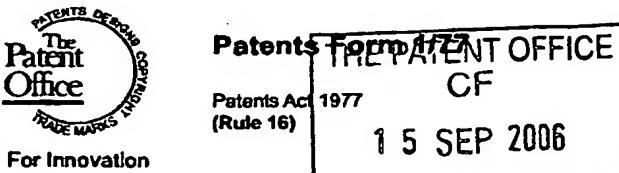
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- 3. Title of the invention: "An Improved Mist Generating Apparatus and Method"
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### An Improved Mist Generating Apparatus and Method

The present invention relates to the field of mist . 1 2 generating apparatus. More specifically, the invention is directed to an improved apparatus and 3 method for generating liquid droplet mists. 4 5 Mist generating apparatus are known and are used in 6 a number of fields. For example, such apparatus are 7 used in both fire suppression and cooling 8 applications, where the liquid droplet mists 9 generated are more effective than a conventional 10 fluid stream. Examples of such mist generating 11 apparatus can be found in WO2005/082545 and 12 WO2005/082546 to the same applicant. 13

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A problem with conventional mist generating apparatus is that not all of the working fluid being used is atomised as it passes through the apparatus. Although the majority of the working fluid is atomised upon entry into the mixing chamber of the apparatus, some fluid is pulled into the chamber but

| 1 | is not atomised. The non-atomised fluid can stick    |
|---|--|
| 2 | to the wall of the mixing chamber and flow           |
| 3 | downstream along the wall to the outlet nozzle,      |
| 4 | where it can fall into the atomised fluid stream.    |
| 5 | This can cause the creation of droplets which are of |
| 6 | non-uniform size. These droplets can then coalesce   |
|   |  |

7 with other droplets to create still larger droplets,

8 thus increasing the problem and creating a mist of

9 non-uniform droplets.

10

In cooling applications in particular, the 11 uniformity of the size of the droplets in the mist 12 is important. In turbine cooling applications, for 13 example, droplets which are over  $10\mu m$  in diameter 14 can cause significant damage to the turbine blades. 15 It is therefore important to ensure control and 16 uniformity of droplet size. Optimally sized 17 droplets will evaporate, thus absorbing heat energy 18 and increasing the air density in the turbine. 19

ensures that the efficiency of the turbine is improved. Existing turbine cooling systems employ

large droplet eliminators to remove large droplets

23 and thus prevent damage to the turbine. However,

such eliminators add to the complexity and

25 manufacturing cost of the apparatus.

26

It is an aim of the present invention to obviate or mitigate one or more of the aforementioned disadvantages.

| <b>-</b> | According to a first aspect of the present invention |
|----------|--|
| 2        | there is provided an apparatus for generating a      |
| 3        | mist, comprising:                                    |
| 4        | a generally cylindrical body; and                    |
| 5        | an elongate member co-axially located within         |
| 6        | the body such that a first transport fluid passage   |
| 7        | and a nozzle are defined between the body and the    |
| 8        | elongate member, the first transport fluid passage   |
| 9        | having a convergent-divergent internal geometry and  |
| 10       | being in fluid communication with the nozzle;        |
| 11       | wherein the elongate member includes a working       |
| 12       | fluid passage and one or more communicating bores    |
| 13       | extending radially outwardly from the working fluid  |
| 14       | passage, the bores allowing fluid communication      |
| 15       | between the working fluid passage and the first      |
| 16       | transport fluid passage; and                         |
| 17       | wherein the one or more communicating bores are      |
| 18       | substantially perpendicular to the first transport   |
| 19       | fluid passage.                                       |
| 20       |  |
| 21       | Preferably, the communicating bore has an inlet      |
| 22       | connected to the working fluid passage and an outlet |
| 23       | connected to the working fluid passage, the outlet   |
| 24       | having a greater cross-sectional area than the       |
| 25       | inlet.   |
| 26       |  |
| 27       | The body has an internal wall having an upstream     |
| 28       | convergent portion and a downstream divergent        |
| 29       | portion, the convergent and divergent portions at    |
| 30       | least in part forming the convergent-divergent       |
| 31       | internal geometry of the first working fluid         |
| 32       | passage. A first end of the elongate member has a    |

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cone-shaped projection, wherein the nozzle is

2 defined between the divergent portion of the internal wall and the cone-shaped projection. 3 one or more communicating bores are adjacent the 4 first end of the elongate member. 5 6 Preferably, the cone-shaped projection has a ramped 7 portion extending upwardly from the surface thereof. 8 9 In a first preferred embodiment, the elongate member 10 further includes a second transport fluid passage 11 having an outlet adjacent the end of the cone-shaped 12 projection. Preferably, the first and second 13 transport fluid passages are substantially parallel. 14 The second transport fluid passage preferably 15 includes an expansion chamber adjacent its outlet. 16 17 In a second preferred embodiment, the bores allowing 18 communication between the working fluid passage and 19 the first transport fluid passage are first bores, 20 and the body further includes a second working fluid 21 22 passage and one or more second communicating bores allowing fluid communication between the second 23 working fluid passage and the first transport fluid 24 passage. Preferably, the second working fluid 25 passage circumscribes the first working fluid 26 27 passage and the first transport fluid passage. Preferably, the second bores are substantially 28 perpendicular to the first transport fluid passage. 29 <sup>1</sup>30 Most preferably, the first and second bores are coaxial. 31 32

5

In a third preferred embodiment, the elongate member 1 further includes: 2 a second transport fluid passage circumscribing 3 the working fluid passage; 4 one or more first communicating bores extending 5 radially outwardly from the working fluid passage, 6 the first bores allowing fluid communication between 7 the working fluid passage and the second transport 8 fluid passage; and 9 10 one or more second communicating bores extending radially outwardly from the second 11 12 transport fluid passage, the second bores allowing fluid communication between the second transport 13 fluid passage and the first transport fluid passage; 14 wherein the first and second communicating 15 16 bores are substantially perpendicular to the second and first transport fluid passages, respectively. 17 18 Preferably, the elongate member further includes a 19 third transport fluid passage adapted to supply 20 transport fluid into the second transport fluid 21 22 passage adjacent the first and second communicating 23 bores. 24 Alternatively, the first transport fluid passage 25 communicates with the nozzle via an outlet and a 26 second transport fluid passage in fluid 27 28 communication with the outlet, wherein the second transport fluid passage has a convergent-divergent 29 internal geometry and is substantially perpendicular 30 to the first transport fluid passage. 31

| 1  | As a further alternative, the apparatus further      |
|----|--|
| 2  | comprises a mixing chamber located between the first |
| 3  | transport fluid passage and the nozzle, and a second |
| 4  | transport fluid passage in communication with the    |
| 5  | mixing chamber and the first transport fluid         |
| 6  | passage, wherein the second transport fluid passage  |
| 7  | is adapted to supply transport fluid to the mixing   |
| 8  | chamber in a direction of flow substantially opposed |
| 9  | to a direction of flow of transport fluid from the   |
| 10 | first transport fluid passage.                       |
| 11 |  |
| 12 | According to a second aspect of the invention, there |
| 13 | is provided a method of generating a mist, the       |
| 14 | method comprising the steps of:                      |
| 15 | supplying a working fluid through a working          |
| 16 | fluid passage;                                       |
| 17 | supplying a first transport fluid through a          |
| 18 | first transport fluid passage;                       |
| 19 | forcing the working fluid from the working           |
| 20 | fluid passage into the first transport fluid passage |
| 21 | via one or more communicating bores extending        |
| 22 | radially outwardly from the working fluid passage;   |
| 23 | accelerating the first transport fluid upstream      |
| 24 | of the communicating bores so as to provide a high   |
| 25 | velocity transport fluid flow; and                   |
| 26 | applying the high velocity transport fluid flow      |
| 27 | to the working fluid exiting the communicating       |
| 28 | bores, thereby imparting a shear force on the        |
| 29 | working fluid and atomising the working fluid to     |
| 30 | produce a dispersed droplet flow regime:             |

| 7          | wherein the high verotity transport fluid flow       |
|------------|--|
| · <b>2</b> | is applied substantially perpendicular to the        |
| 3          | working fluid flow exiting the bores.                |
| 4          |  |
| 5          | Preferably, the method further includes the steps    |
| 6          | of:  |
| 7          | forcing the atomised working fluid from the          |
| 8          | first transport fluid passage into a second          |
| 9          | transport fluid passage via one or more second       |
| 10         | communicating bores extending radially outwardly     |
| 11         | from the first transport fluid passage;              |
| 12         | supplying a second transport fluid through the       |
| 13         | second transport fluid passage;                      |
| 14         | accelerating the second transport fluid              |
| 15         | upstream of the second communicating bores so as to  |
| L <b>6</b> | provide a second high velocity transport fluid flow; |
| L7         | and  |
| L8         | applying the second high velocity transport          |
| L <b>9</b> | fluid flow to the atomised working fluid exiting the |
| 20         | second communicating bores, thereby imparting a      |
| 21         | second shear force on the atomised working fluid and |
| 22         | further atomising the working fluid;                 |
| 23         | wherein the second high velocity transport           |
| 24         | fluid flow is applied substantially perpendicular to |
| 25         | the atomised working fluid flow exiting the second   |
| 26         | bores.   |
| 27         | •  |
| 8          | Preferred embodiments of the present invention will  |
| 9          | be described, by way of example only, with reference |
| 0          | to the accompanying drawings, in which:              |
| . 7        |  |

| 1   | Figures 1(a)-1(e) show detail section views          |
|-----|--|
| 2   | through a first embodiment of a mist generating      |
| 3   | apparatus;   |
| 4   | Figure 2 shows a detail section view through a       |
| . 5 | second embodiment of a mist generating apparatus;    |
| 6   | Figure 3 shows a section view through a third        |
| 7   | embodiment of a mist generating apparatus;           |
| 8   | Figures 4(a)-4(c) show detail section views          |
| 9   | through a fourth embodiment of a mist generating     |
| 10  | apparatus;   |
| 11  | Figure 5 shows a detail section view through a       |
| 12  | fifth embodiment of a mist generating apparatus;     |
| 13  | Figure 6 shows a detail section view through a       |
| 14  | sixth embodiment of a mist generating apparatus; and |
| 15  | Figure 7 shows a detail section view through a       |
| 16  | seventh embodiment of a mist generating apparatus.   |
| 17  |  |
| 18  | Figure 1(a) shows a first embodiment of mist         |
| 19  | generating apparatus according to the present        |
| 20  | invention. The apparatus, generally designated 10,   |
| 21  | comprises a generally cylindrical body 12 and an     |
| 22  | elongate member 14 projecting co-axially within the  |
| 23  | body 12. The member 14 and body 12 are so arranged   |
| 24  | that a first transport fluid passage 16 and a nozzle |
| 25  | 32 are defined between the two. The body 12 has an   |
| 26  | internal wall 18 which includes a convergent portion |
| 27  | 20 upstream of a divergent portion 22. The elongate  |
| 28  | member 14 has an external wall 24 which is           |
| 29  | substantially straight and parallel to the           |
| 30  | longitudinal axis L shared by the body and elongate  |
| 31  | member. As Figure 1(a) is only a detail view, it     |
| 32  | will be appreciated that the entire apparatus is not |

illustrated in this figure. As the body 12 is 1 generally cylindrical, a further portion of the body 2 12, mirrored about the longitudinal axis L, is 3

present below the elongate member 14, but is not 4

shown in Figure 1(a) for reasons of clarity. Thus, · 5

passage 16 is an annular passage surrounding the 6

elongate member 14. The elongate member 14 ends in 7

a cone-shaped projection 15. 8

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The elongate member 14 includes a passage 26 for the 10

introduction of a working fluid. The passage will 11

therefore be referred to as the working fluid 12

passage 26. The passage 26 extends along the length 13

of the elongate member 14 and is also co-axial with 14

the body 12 and elongate member 14. The passage 26 15

is blind, in that it ends in a cavity 28 located in 16

the outer cone portion 15 of the elongate member 14. 17

Extending radially outwardly from the passage 26 in 18

a direction substantially perpendicular to the 19

transport fluid passage 16 are one or more 20

communicating bores 30. These bores 30 allow fluid 21

communication between the working fluid passage 26 22

and the transport fluid passage 16. The outer cone 23

portion 15 of the elongate member 14 and the 24

divergent portion 22 of the internal wall 18 define 25

a mixing chamber 19 which opens out into a nozzle 32 26

through which fluid is sprayed. 27

28

The operation of the first embodiment will now be 29

described. A working fluid, such as water for 30

example, is introduced from a working fluid inlet 31

(not shown) into the working fluid passage 26. 32

| _         | working ridia from along the passage 20 until        |
|-----------|--|
| 2         | reaching the cavity 28. Upon reaching the cavity     |
| 3         | 28, the working fluid is forced through the bores 30 |
| 4         | into the transport fluid passage 16. A transport     |
| 5         | fluid, such as steam for example, is introduced from |
| 6         | a transport fluid inlet (not shown) into the         |
| 7         | transport fluid passage 16. Due to the convergent-   |
| 8         | divergent section of the passage 16 formed by the    |
| 9         | convergent and divergent portions 20,22 of the body  |
| LO -      | 18, the passage acts as a venturi section,           |
| 11        | accelerating the transport fluid as it passes        |
| <b>.2</b> | through the convergent-divergent section into the    |
| 13        | mixing chamber 19. This acceleration of the          |
| 4         | transport fluid ensures that the transport fluid     |
| .5        | flows past the ends of the bores 30 at very high,    |
| .6        | possibly even supersonic, velocity.                  |
| .7        |  |
| .8        | With the transport fluid flowing at such high        |
| 9         | velocity and the working fluid exiting the bores 30  |
| 0         | into the passage 16 in a direction substantially     |
| 1         | perpendicular to the transport fluid flow, the       |
| 2         | working fluid is subjected to very high shear forces |
| 23        | by the transport fluid. Droplets are sheared from    |
| 4         | the working fluid flow as it exits the bores 30      |
| 5         | producing a dispersed droplet flow regime. The       |
| 6         | atomised flow is then carried out through the mixing |
| 7         | chamber 19 to the nozzle 32. In such a manner, the   |
| 8         | apparatus 10 creates a flow of substantially uniform |
| 9         | sized droplets from the working fluid.               |
| 0         |  |
| 1         | Figures 1(b)-1(e) show potential modifications to    |
| 2         | the nozzle 32 adjacent the outlet of the bores 30:   |

Figures 1(b)-1(d) show nozzles where the outlet of 2 the bore 30 has a greater cross-sectional area than the inlet 29 communicating with the working fluid 3 passage 26. In Figure 1(b) the bore 30 has a curved 4 outward taper at the outlet 31b which provides the 5 outlet 31b with a bowl-shaped profile when viewed in 6 section. In Figure 1(c), a similar arrangement is 7 shown, but here the expanded diameter of the outlet 8 31c is achieved by providing a stepped portion 9 10 rather than a gradual outward taper. With the nozzle of Figure 1(d), the bore 30 gradually tapers 11 12 outwards along the length thereof from inlet 29 to 13 outlet 31d. 14 15 By providing bores 30 whose outlets 31b,31c,31d are 16 of greater diameter than their respective inlets 29, 17 an area of lower pressure is provided in the working fluid as it leaves the outlets 31b, 31c, 31d. This 18 has the effect of presenting a greater surface area 19 of working fluid to the transport fluid in the 20 mixing chamber 19, thereby further increasing the 21 shear effect of the transport fluid on the working 22 fluid. Additionally, the expansion of the bores 30, 23 24 particularly in the cases of the Figure 1(b) and 1(c) nozzles, will increase the turbulence of the 25 26 working fluid flow as it exits the bores 30, 27. limiting the potential for any of the working fluid flow to become trapped along the walls of the bores 28 30. 29 30 As explained above, one undesirable phenomenon in 31 mist generating apparatus is that some of the 32

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working fluid is not instantly atomised upon exit

from the bores 30. In such instances, the non-2 atomised fluid can flow along the wall of the outer 3 cone portion 15 of the nozzle 32 and then disrupt 4 the size of the working fluid droplets which have 5 already been atomised. This phenomenon can be 6 avoided in the nozzle shown in Figure 1(e). With 7 this nozzle, the wall of the outer cone portion 15 8 is provided with a ramped portion 34 which extends 9 10 upwardly from the outer cone wall to a peak, also known as a surface separation point. Any non-11 12 atomised fluid flow along the outer cone 15 will flow up the ramped portion 34. Once the fluid flow 13 arrives at the peak, it will be subjected to the 14 15 shear forces of the transport fluid, will atomise, and then join the remainder of the droplets as they 16 exit the nozzle 32. 17 18 19 Figure 2 shows a second embodiment of the apparatus, 20 which also solves the same problem as the modified 21 nozzle of Figure 1(e). In this instance, the 22 elongate member 14 includes a working fluid passage 26 as before. However, instead of passing through 23 the central axis of the elongate member 14 as in the 24 25 previously described embodiments, in this embodiment the working fluid passage 26 is arranged so as to 26 27 circumscribe a second transport fluid passage 40 located along the longitudinal axis of the elongate 28 member 14. The purpose of the second transport 29 fluid passage 40 is to ensure any non-atomised fluid 30 which flows down the surface of the outer cone 15 is 31 32 atomised when it reaches the outlet 42 of the

passage 40, which is adjacent the end of the outer 1 cone 15. Thus, transport fluid flows through both 2 the first transport fluid passage 16 and the second 3 transport fluid passage 40. The second transport 4 5 fluid passage 40 can include an expansion chamber 44 if desired, and is preferably substantially parallel 6 to the first transport fluid passage 16. 7 8 A third embodiment of the apparatus is shown in Figure 3. This embodiment shares a number of 10 features with the first embodiment described above. 11 As a result, these features will not be described 12 again in detail here, but have been assigned the 13 same reference numbers, where appropriate. The 14 first difference between the first and third 15 embodiments is that the external wall 24' of the 16 elongate member 14 is of the same convergent-17 divergent geometry as the internal wall 18 of the 18 19 Hence, the convergent and divergent body 12. 20 portions 20,22 of the internal wall 18 are mirrored by identical portions of the external wall 24' of 21 the elongate member 14. As a result, both walls 22 18,24' define a throat section 50 in the first 23 transport fluid passage 16. 24

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The second key difference between the third embodiment of the apparatus and the preceding embodiments is that as well as having a first working fluid passage 26 along the centre of the elongate member 14, a second working fluid passage 52 is also provided in the body 12, the second working fluid passage 52 circumscribing both the

| 1   | first working fluid passage 26 and the transport     |
|-----|--|
| 2   | fluid passage 16. This means that working fluid is   |
| 3   | supplied into the mixing chamber 19 from both first  |
| 4   | and second bores 30,54 which extend radially         |
| 5   | outwardly from their respective passages 26,52 and   |
| 6   | connect the first and second working fluid passages  |
| 7   | 26,52 with the transport fluid passage 16. As with   |
| 8   | the first working fluid passage 26, the second       |
| 9   | working fluid passage 52 is also blind, with a       |
| 10  | cavity 56 located at the end of the passage 52       |
| 11  | remote from the working fluid inlet (not shown).     |
| 12  | The first and second bores 30,54 are preferably co-  |
| 13  | axial, as seen in section in Figure 3. This ensures  |
| 14  | that the working fluid enters the transport fluid    |
| 15  | passage 16 at the same point from both the first and |
| 16  | second working fluid passages 26,52. The first and   |
| L7  | second bores 30,54 are substantially perpendicular   |
| 18  | to the transport fluid passage 16.                   |
| 19  | ·<br>-   |
| 20  | The third embodiment will operate in substantially   |
| 21  | the same manner as that described in respect of the  |
| 22  | first embodiment. Working fluid exiting the first    |
| 23  | and second bores 30,54 will be sheared by the        |
| 24  | transport fluid flowing through the transport fluid  |
| 25  | passage 16, thereby creating a mist of uniform sized |
| 26  | droplets.  |
| 27  | ·  |
| 8.8 | A fourth embodiment of the invention is illustrated  |
| 9   | in Figure 4(a). Again, the basic layout of the       |
| 0   | apparatus is the same as with the first embodiment,  |
| 1   | so like features have been again assigned the same   |
| 2   | reference numbers. The elongate member 14 has a      |

- central working fluid passage 26 which ends in a cavity 28 remote from a working fluid inlet (not shown). A first transport fluid passage 16 is
- 4 defined by an external wall 24 of the elongate
- 5 member 14 and convergent and divergent portions
- 6 20,22 of the internal wall 18 of the body 12.
- 7 Again, it will be appreciated that Figure 4(a) only
- 8 illustrates half of the apparatus, with the half not
- 9 illustrated being a mirror image about the
- 10 longitudinal axis L of the illustrated portion.

- 12 The elongate member 14 of this fourth embodiment is
- adapted to include a second transport fluid passage
  - 14 60 circumscribing the central working fluid passage
  - 15 26. The transport and working fluid passages 60,26
  - 16 are co-axial about the longitudinal axis L. With
  - the second transport fluid passage 60 circumscribing
- 18 the working fluid passage 26, the second transport
- 19 fluid passage lies between the working fluid passage
- 20 26 and the first transport fluid passage 16. A
- 21 number of first bores 62 allow fluid communication
- 22 between the working fluid passage 26 and the second
- 23 transport fluid passage 60. A number of second
- 24 bores 64 allow fluid communication between the
- 25 second transport fluid passage 60 and the first
- transport fluid passage 16.

- In operation, working fluid is forced through the
- 29 first bores 62 into the second transport fluid
- 30 passage 60, where transport fluid shears the working
- 31 fluid entering the passage perpendicular to the
- 32 transport fluid flow. The resultant atomised fluid

then flows through the second bores 64 into the 1 2 first transport fluid passage 16, whereupon it is sheared for a second time by a second flow of 3 transport fluid. Providing two locations at which 4 the working fluid is subjected to the shear forces 5 of the transport fluid allows the apparatus to 6 generate still smaller droplet sizes. 7 8 9 Figures 4(b) and 4(c) illustrate examples of communicating bores 70,72 which are not 10 perpendicular to the flow of transport fluid through 11 the transport fluid passage 16. The bore 70 of 12 Figure 4(b) presents fluid into the transport fluid 13 flow at an angle of less than 90 degrees such that 14 the fluid flows against the flow of transport fluid. 15 16 Such an arrangement increases the shear forces on the working fluid from the transport fluid. In 17 Figure 4(c) the bore 72 is at an angle of over 90 18 19 degrees, so that the fluid flow is at an angle to 20 the transport fluid flow, but is not perpendicular thereto. This arrangement reduces the amount of 21 22 shear imparted on the working fluid by the transport fluid. 23 A fifth embodiment of the invention is illustrated in Figure 5. The elongate member 14 has a central working fluid passage 26 which ends in a cavity 28 remote from a working fluid inlet (not shown). A

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25 26 27 28 first transport fluid passage 16 is defined by an 29 30 external wall 24 of the elongate member 14 and convergent and divergent portions 20,22 of the 31 internal wall 18 of the body 12. 32 In this

embodiment, the external wall 24 of the elongate 1 2 member 14 tapers outwardly in the direction of the mixing chamber 19 and nozzle 32 until it reaches one 3 or more second bores 64. Again, it will be 4 appreciated that Figure 5 only illustrates half of 5 the apparatus, with the half not illustrated being a 6 mirror image about the longitudinal axis L of the 7 illustrated portion. 8 9 The elongate member 14 of this fourth embodiment is 10 adapted to include a second transport fluid passage 11 60 circumscribing the central working fluid passage 12 The transport and working fluid passages 60,26 13 are co-axial about the longitudinal axis L. With 14 the second transport fluid passage 60 circumscribing 15 the working fluid passage 26, the second transport 16 fluid passage lies between the working fluid passage 17 26 and the first transport fluid passage 16. One or 18 more first bores 62 allow fluid communication 19 20 between the working fluid passage 26 and the second transport fluid passage 60. One or more of the 21 22 second bores 64 allow fluid communication between the second transport fluid passage 60 and the first 23 transport fluid passage 16. 24 25 A further difference between the fifth embodiment 26 27 and the preceding fourth embodiment in particular is that a third transport fluid passage 80 is provided 28 in the elongate member 14. The third transport 29 fluid passage 80 may receive transport fluid from 30 the same source as the first and second transport 31 32 fluid passages 16,60, or else it may have its own

dedicated transport fluid source (not shown). The 1 third transport fluid passage 80 has an outlet 82 2 which is on the downstream side of the first bore(s) 3 62. As a result, the outlets of the second and 4 5 third transport fluid passages 60,80 are positioned either side of the first bores 62 and open into the 6 second bores 64. 7 8 9 In operation, working fluid is forced through the first bores 62 from the working fluid passage 26, 10 11 where transport fluid from the second and third 12 transport fluid passages 60,80 shears the working The resultant atomised fluid then flows 13 fluid. 14 through the second bores 64 into the first transport fluid passage 16, whereupon it is sheared for a 15 second time by a second flow of transport fluid. 16 Providing two locations at which the working fluid 17 is subjected to the shear forces of the transport 18 19 fluid allows the apparatus to generate still smaller 20 droplet sizes. By providing two sources of 21 transport fluid from the second and third transport 22 fluid passages 60,80 adjacent the first bore(s) 62, 23 even smaller droplets of the working fluid can be obtained due to the effective twin shear action of 24 the transport fluid on the working fluid prior to 25 the atomised fluid entering the second bore(s) 64 26 and being further atomised. **27** '

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Figures 6 and 7 show sixth and seventh embodiments of the apparatus, respectively, in which secondary shear actions take place in the manner of the fourth and fifth embodiments described above. In the sixth

embodiment shown in Figure 6, the elongate member 14 has a central working fluid passage 26 which ends in 2 3 a cavity 28 remote from a working fluid inlet (not shown). A first transport fluid passage 16 is 4 defined by an external wall 24 of the elongate 5 member 14 and convergent and divergent portions 6 20,22 of the internal wall 18 of the body 12. The 7 external wall 24 of the elongate member 14 runs 8 substantially parallel to the transport fluid 9 passage 26. One or more first bores 62 allow fluid 10 communication between the working fluid passage 26 11 and the first transport fluid passage 16. 12 13 The key difference between the sixth embodiment and 14 15 the fifth embodiment in particular is that a second transport fluid passage 90 is provided, but in this 16 17 case the second transport fluid passage 90 is substantially perpendicular to the first transport 18 fluid passage 16. The second transport fluid 19 passage 90 may receive transport fluid from the same 20 21 source as the first transport fluid passage 16, or 22 else it may have its own dedicated transport fluid 23 source (not shown). In this embodiment, the first transport fluid passage 16 has an outlet 17 in 24 communication with the second transport fluid 25 passage 90. A mixing chamber 19 is defined where 26 the first and second transport fluid passages 16,90 27 28 meet one another. The second transport fluid passage 90 has a convergent-divergent internal 29 geometry upstream of the first transport fluid 30 passage outlet 17, thereby ensuring that the 31 32 transport fluid passing through the passage 90 is

accelerated prior to meeting the atomised fluid exiting the first transport fluid passage 16.

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4 In operation, working fluid is forced through the

first bores 62 from the working fluid passage 26,

6 where transport fluid from the first transport fluid

7 passage 16 shears the working fluid. The resultant

8 atomised fluid then flows through the outlet 17 into

9 the second transport fluid passage 90, whereupon it

is sheared for a second time by the second flow of

11 transport fluid.

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13 The seventh embodiment of the invention differs from

14 the sixth embodiment in that the second transport

15 fluid passage 100 is arranged such that the

16 direction of the second transport fluid flow is

17 generally opposite to the flow of transport fluid

through the first transport fluid passage 16. As

19 before, both the first and second transport fluid

20 passages 16,100 have convergent-divergent internal

21 geometry.

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Working fluid exits the working fluid passage 26 via

first bore(s) 62 in a flow direction perpendicular

to the first transport fluid passage 16. Transport

fluid accelerated through the passage 16 shears the

working fluid exiting the bore(s) 62, creating an

atomised fluid flow. The atomised fluid flow,

29 flowing in the direction indicated by arrow D1, then

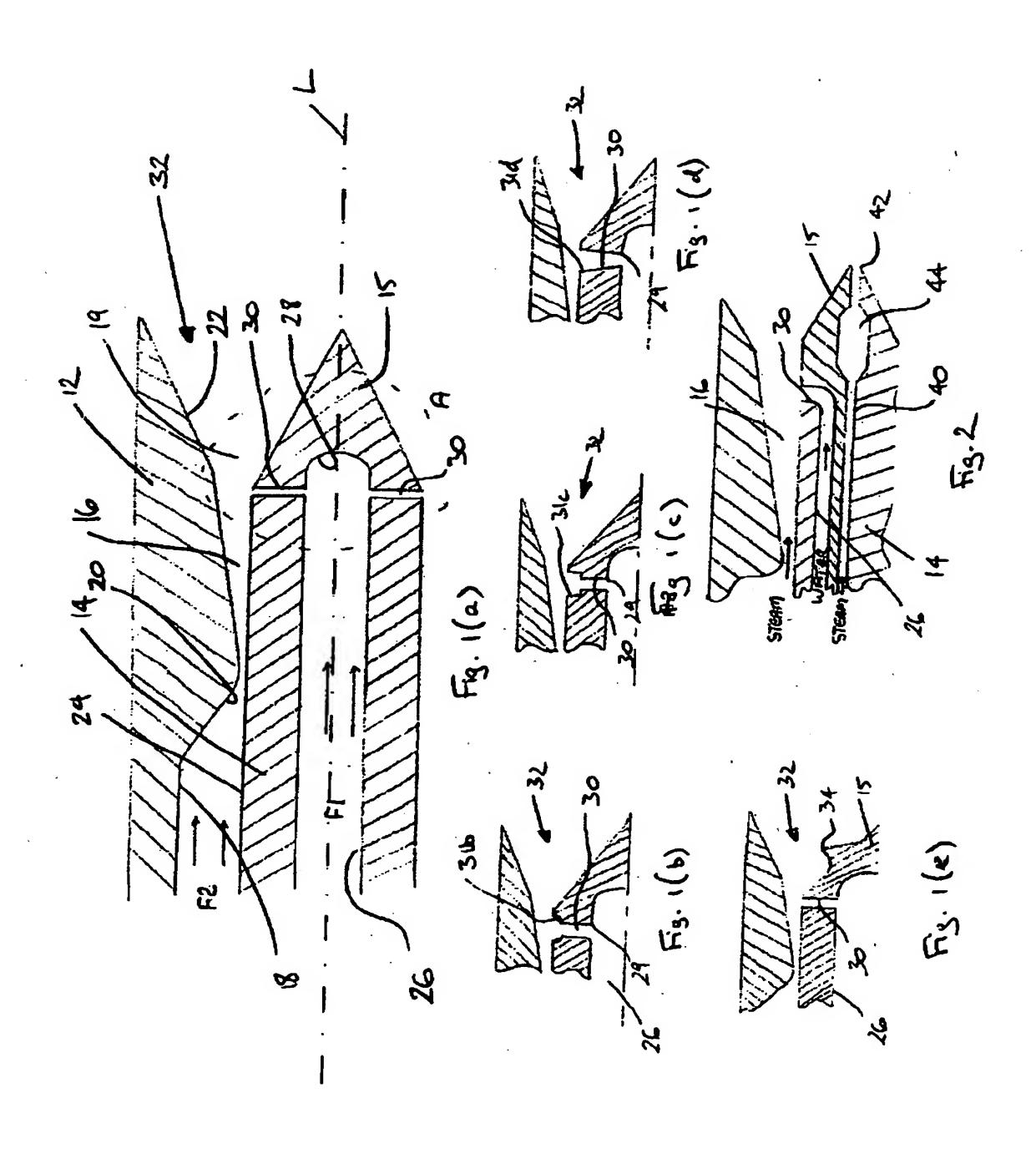
30 meets the accelerated secondary transport fluid

31 flow, illustrated by arrow D2, at a mixing chamber

32 19. The two fluid flows D1, D2 combine in the mixing

chamber 19 to further atomise the working fluid prior to the atomised working fluid exiting via 2 outlet 104. 3 4 The purpose of the sixth and seventh embodiments is 5 to shear the working fluid once and then carry the 6. droplets into a further stream of transport fluid 7 where the velocity of the droplets is reduced. 8 allows the production of uniform droplets by 9 shearing with a first, preferably supersonic, stream 10 of transport fluid and then reducing the velocity of 11 the stream with the second transport fluid flow. 12 These embodiments are for use in applications which 13 require small droplet size but low projection 14 velocities. 15 16 Each of the embodiments described here uses the 17 generally perpendicular arrangement of the working 18 fluid bores and transport fluid passages to obtain a 19 crossflow of the transport and working fluids. 20 crossflow (where the two fluid flows meet at 21 approximately 90 degrees to one another) ensures the 22 penetrative atomisation of the working fluid as the 23 transport fluid breaks up the working fluid. 24 natural Kelvin-Helmholtz/Rayleigh Taylor 25 instabilites in the working fluid as it is forced 26 into an ambient pressure environment also assist the 27 atomisation of the working fluid. 28 29 Furthermore, by locating the elongate member 14 30 along the centre of the apparatus, the atomised 31 working fluid exits the apparatus via an annular 32

nozzle which circumscribes the elongate member. 1 2 elongate member effectively blocks the centre of the nozzle, which provides a further geometric mechanism 3 to assist the atomisation of the working fluid. 4 blocking of the centre of the nozzle creates a low 5 pressure recirculation zone adjacent the nozzle cone 6 As the high-speed atomised working fluid exits 7 the annular nozzle it imparts further shear forces 8 on the droplets in the recirculation zone, leading 9 to a further atomisation of the working fluid. 10 11 In the fifth embodiment shown in Figure 5, the 12 method of operation may be adapted by swapping the 13 functions of the fluid passages 26,60,80. In other 14 words, the passage 26 could supply the transport 15 fluid, whilst the passages 60,80 supply the working 16 fluid. In an alternative adaptation of the 17 apparatus of the fifth embodiment, the apparatus 18 could be adapted to feed gas bubbles through the 19 first bores 62 as the working fluid passes through. 20 This has the effect of breaking up the working fluid 21 stream prior to atomisation and also increasing 22 turbulence in the working fluid, both of which help 23 improve the atomisation of the working fluid in the 24 25 apparatus. 26 Further modifications and improvements may be 27 incorporated without departing from the scope of the 28 invention. 29



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